Alkali compounds catalyzed low temperature methanol synthesis over Cu-based catalyst

BAOSHAN HU Department of Chemical Processes and Environments, Faculty of Environmental Engineering, The University of Kitakyushu, 1-1, Hibikino, Wakamatsu, Kitakyushu, JAPAN http://www.hotmail.com

Abstract: -A novel mixed catalyst system containing alkali compounds over Cu/MgO-Na catalyst was developed to synthesize methanol from syngas via ethyl formate in a slurry reactor. The results exhibited that among the used alkali formates (HCOOM, M=Li, Na, Cs, Ca, Ba), sodium formate showed the optimizing catalytic function with Cu/MgO-Na catalyst, and high CO conversion(>80%) and methanol selectivity(\sim 90%) with a mass space velocity of 1800L(STP)/h.kg was achieved at low temperature of 433K and 5.0Mpa. In addition, Na₂CO₃, NaHCO₃ and NaOH could catalyze the methanol synthesis through their transformation into HCOONa.

Key-Words: - CuMgO-Na/HCOONa catalysis system, slurry phase, low temperature methanol synthesis,

1 Introduction

Methanol is an industrially important chemical, it is produced at an annual rate of over 20 million tons worldwide. Methanol is widely used as a feedstock in various chemical applications and also be used as a transportation fuel or a fuel additive. It is also the raw resource for other important chemicals, such as MTBE, which is a rapidly growing octane enhancer for the automotive market.

The efficiency of methanol synthesis in the industrial process is severely limited bv thermodynamics because methanol synthesis is an extremely exothermic reaction ($\Delta H = -91 \text{KJ/mol}$). To overcome the disadvantage, an alternative methanol synthesis method via methyl formate (MeF) at low temperatures in liquid phase had been proposed by Christiansen[1], and was widely studied by many researchers. The process involved carbonylation of methanol to methyl formate (MeF) (CH3OH+CO= HCOOCH3) and hydrogenolysis of MeF to methanol (HCOOCH3+H2=2CH3OH).The reactions two proceeded in one reactor, which was so-called concurrent process. In which, the catalyst for carbonylation was usually homogeneous alkali metal methoxide, however, it can be easily poisoned by

CO2 and H2O; the catalyst for hydrogenolysis was often modified copper solid catalyst.

In the present study, highly active system of different kinds of alkali compounds over Cu-based catalyst for low temperature methanol synthesis LTMS) was studied.

2 Experimental

The catalyst was prepared by the conventional co-precipitation method. A mixing aqueous solution of copper nitrate and magnesium nitrate was used to produce the precipitate. The obtained precipitation was filtrated, washed, dried. Subsequently, the precursor was impregnated with sodium carbonate. The impregnated Cu-based catalyst was finally reduced in a stream of H2 at 523K for 2h before its activity evaluation.

co-precipitation method. A mixing aqueous solution of copper nitrate and magnesium nitrate was used to produce the precipitate. The obtained precipitation was filtrated, washed, dried. Subsequently, the precursor was impregnated with sodium carbonate. The impregnated Cu-based catalyst was finally reduced in a stream of H2 at 523K for 2h before its activity evaluation. A flow-type semi-batch autoclave reactor with an inner volume of 85ml was employed in the experiment. The stirring speed was 1660 rpm to prevent the occurrence of the diffusion-controlled regime. All products were analyzed by two gas chromatographs, where GC-8A/TCD (Shimadzu) was used for gas products and GC353/FID(GL Science) was used for liquid products[2].

3 Results and discussion

Several alkali formats were chosen as carbonylation catalysts for low temperature methanol synthesis over present Cu/MgO-Na catalyst. The standard reaction conditions here were as follows: H2/CO/Ar=64.5/32.5/3, temperature=433K, pressure =5.0MPa, solvent=ethanol, W/F=12.44g.h.mol-1, concentration of alkali compounds=0.33mol/L, reaction time=24hours. Fig.1 showed the corresponding reaction activity, formation rate of methanol and selectivity of main by-products.

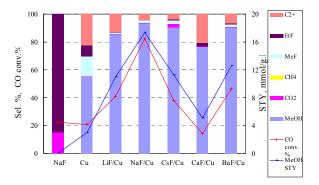
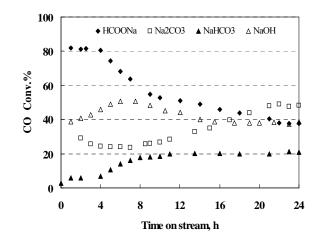


Fig.1 Alkali formates as carbonylation catalysts for low temperature methanol synthesis over Cu-based catalyst

Sodium formate exhibited low activity for carbonylation of methanol, only CO₂ and ethyl formate were products. Cu/MgO-Na catalyst gave a lower catalytic function for methanol synthesis under present reaction conditions, and methanol selectivity was about 56%. However, in the alkali formats/Cu catalyst systems, methanol synthesis showed higher reaction activities and methanol selectivity, like HCOOLi, HCOONa, HCOOCs. Especially, HCOONa/Cu system had a highest reaction activity among the three systems, it might attribute to the



42

Fig.2 Catalytic performance of alkali compounds for LTMS in liquid phase over Cu/MgO-Na catalyst

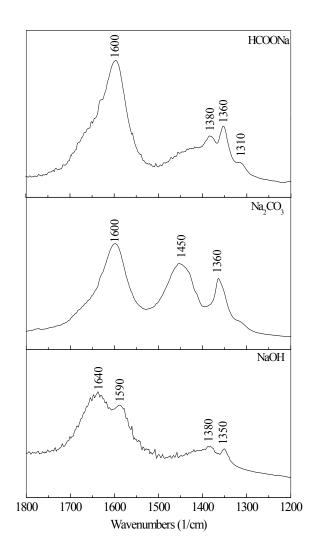


Fig.3 FT-IR spectra for solid sample in liquid phase after reaction using HCOONa, Na₂CO₃, NaOH over Cu/MgO-Na catalyst

dissociation activity of dissolved alkali formats and their size match degree of ions radius with Cu catalyst[3]. Differently, for II A Group formates, as shown Ca(HCOO)₂ and Ba(HCOO)₂, the corresponding catalytic function descended. But, their stabilities were better than those of alkali formats.

Under the same reaction conditions, other several alkali compounds, like Na₂CO₃, NaHCO₃ and NaOH, were chosen for the carbonylation catalysts. For comparison, their CO conversions function with the time on stream were shown in Fig.2. In the case of Na2CO3, during the initial hours the activity was lower and then increased to a stable level; in the case of NaHCO3, the activity quickly increased to a stable level. It indicated that NaHCO3 almost had no catalytic function on present low temperature methanol synthesis. And in the case of NaOH with strong basicity, reaction activity was also showed. During the early hours, CO conversion was slowly increased and then went along the tendency similar with that in the case of HCOONa. After more than 20 hours, the CO conversions were almost same at about 38%. There was no doubt that the same reaction activity would kept from the 20th hours on. Therefore, catalytic sites should either be same or be inter-transformed into each other with a dynamic equilibrium after some reaction hours when using HCOONa and NaOH.

The results that Na₂CO₃ and NaOH both emerged the considerable reaction activities with HCOONa made it meaningful to make clear their roles and relative inter-transformations in present system. Solid materials attained by vaporizing the final liquid sample after reaction with HCOONa, Na₂CO₃ and NaOH, respectively, were qualitatively analyzed by FTIR, shown in Fig.3. Assignments of the bands were made by analogy with the spectra of known compounds and by comparison with published literatures. For HCOONa, the bands at 1600 cm⁻¹ and 1360 cm⁻¹ were antisymmetric and symmetric stretching vibrations of carbon-oxygen bands, respectively, they were the label bands of HCOONa. Besides, the bands at 1380 cm⁻¹ and 1310cm⁻¹ resulted from the NaHCO₃. It illuminated that some fraction of HCOONa was transformed into NaHCO₃, which might result in the deactivation of HCOONa comparing with the reaction activity of NaHCO₃ in Fig.1. For Na₂CO₃, the band at 1450 cm-1 was ascribed to Na₂CO₃. Moreover, the bands of HCOONa were detected out, which contributed to gradually increasing reaction activity of Na₂CO₃. For the case of NaOH, the bands at 1640 cm-1, 1420 cm-1 and 1380 cm-1 belonged to NaHCO₃, the bands at 1600 cm-1 and 1360 cm-1 were attributed to HCOONa. The results demonstrated that NaOH was transformed into HCOONa and NaHCO3 after It explained that NaOH showed reaction. comparative reaction performance of with that HCOONa[4].

4 Conclusion

The alternative alkali compounds like HCOONa, Na₂CO₃ and NaOH instead of conventional CH₃ONa over Cu-cased catalyst showed high performance for low temperature methanol synthesis in liquid phase. Alkali carbonate and alkali hydroxide were both transformed into alkali formate to catalyze the process, formate was the substaintial species for the current process. It exploited a novel route concerning about utilization of other alkali compounds and optimization of relative transformation equilibrium for LTMS in liquid phase.

References

1.Christiansen, J.A., 1919. Assigned U.S.Patent, 1 302 011

2.Noritatsu T, J.Q Zeng, Yoshiharu Yoneyama, Kaoru Fujimoto. Catal. Comm.2(2001) 213-217

3.S.P.Tonner, M.S.Wainwright, D.L.Trimm and N.W.Cant. J.Mol.Catal.18(1983) 215

4. Yang R.Q., Zhang Y., Yuki I., Noritatsu T. Applied Catalysis A:General288(2005) 126-133